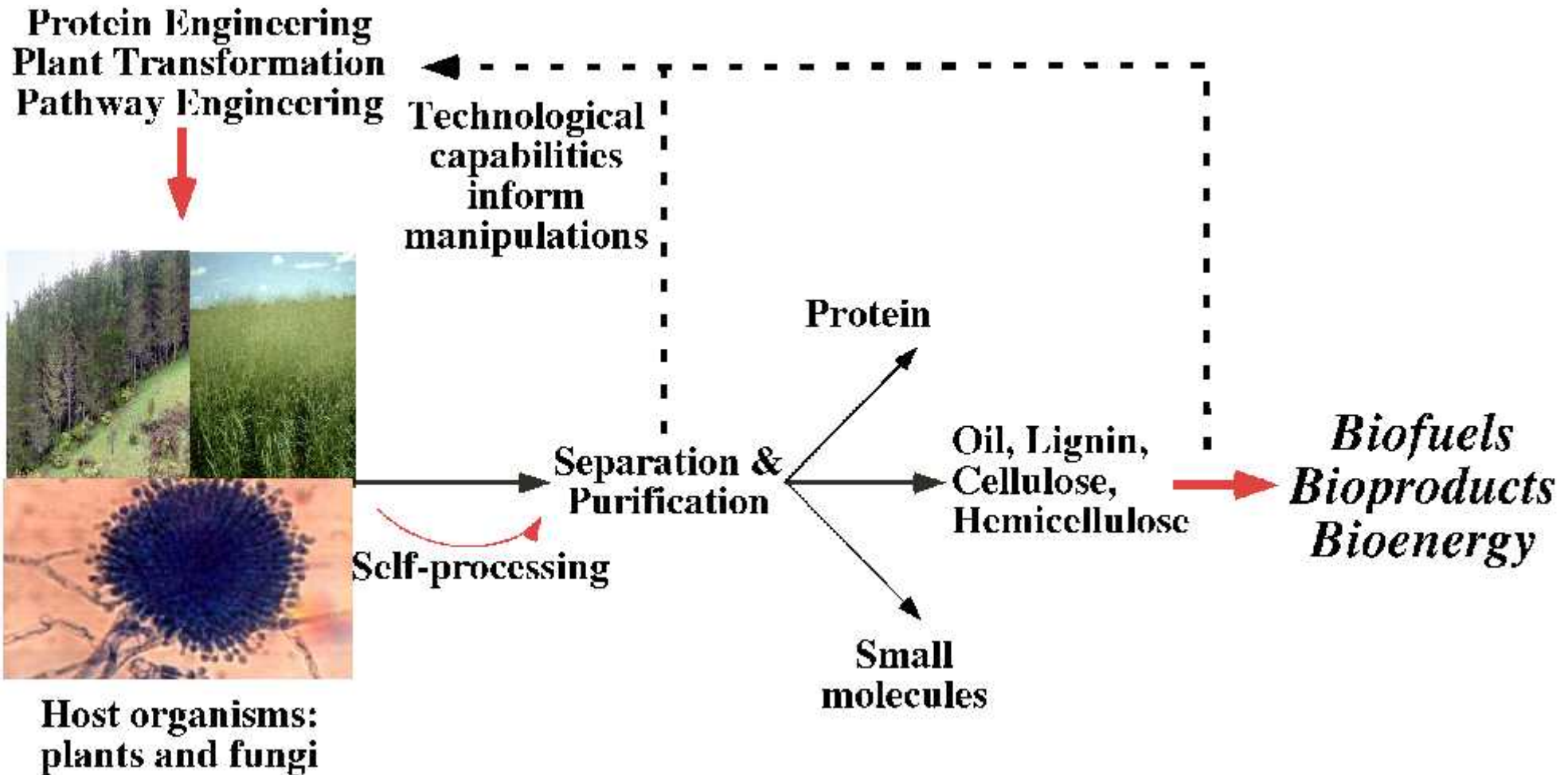


Biochemical Technologies for Biofuel Production: Challenges and Opportunities

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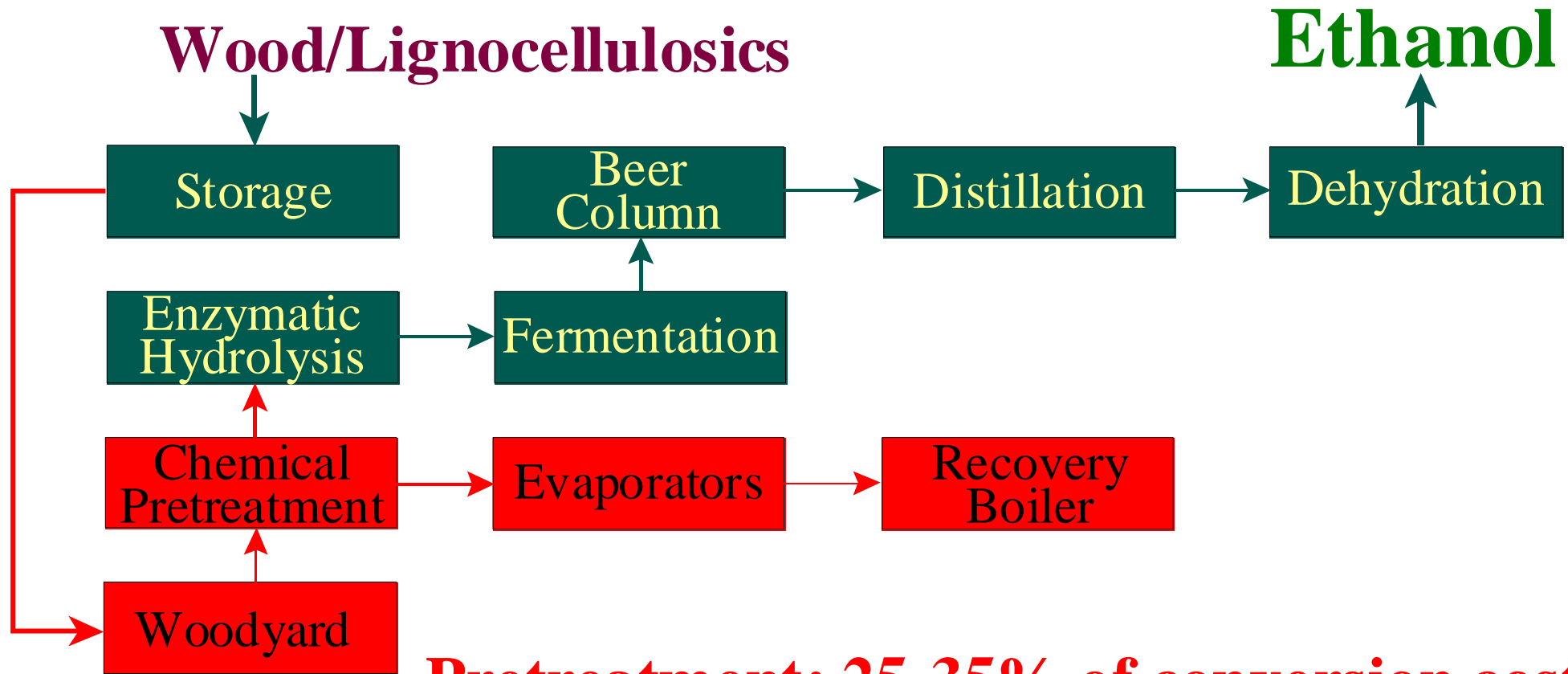
Advanced Energy 2009

There are several opportunities upstream and downstream for biochemical processing



Conversion of traditional lignocellulosics to ethanol

(Chemical pretreatment + enzymatic saccharification + fermentation)



Pretreatment: 25-35% of conversion cost

Pretreatment is necessary because lignin in plant cell walls limits enzyme's accessibility to polysaccharides.

Upstream Processing: Making “better” biomass

**Antisense *4CL*-
mediated lignin
reduction
in Trees**

Aspen
Hybrid poplar
Eucalyptus
Loblolly pine



Genetic Engineering of Lignin Synthesis in Trees

Normal
wood

Genetically
modified
wood

Cellulose

43%

54%

Lignin

22%

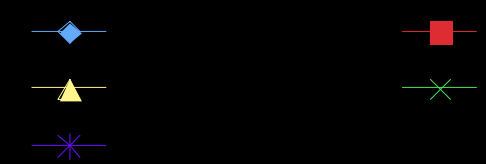
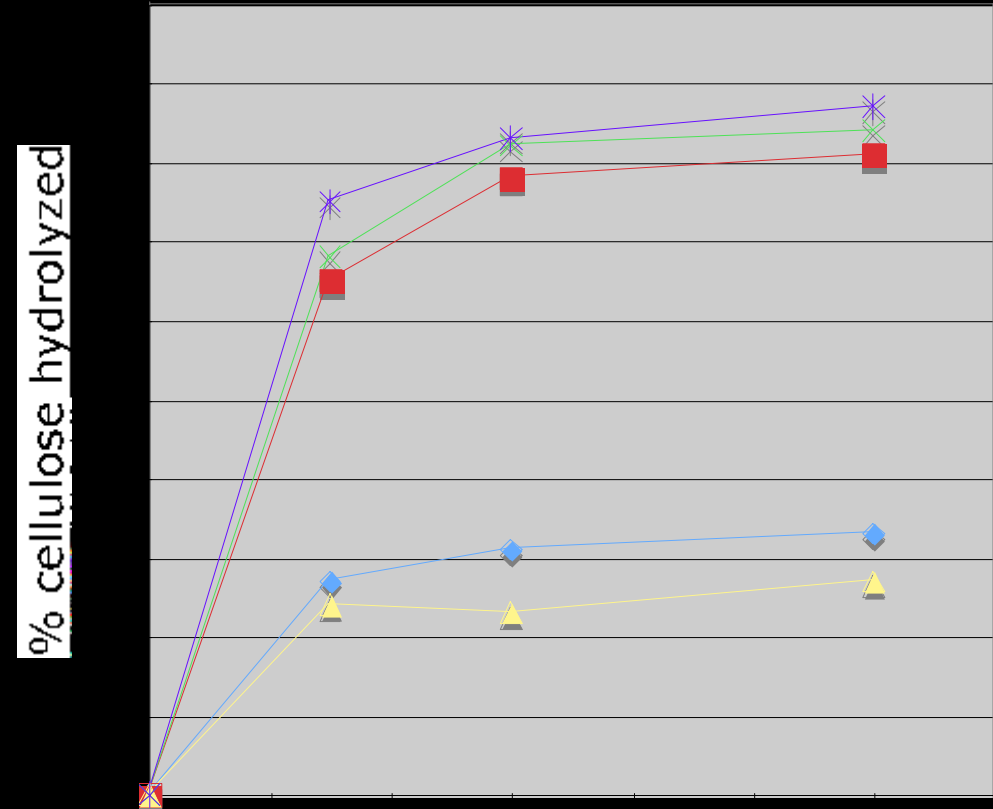
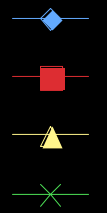
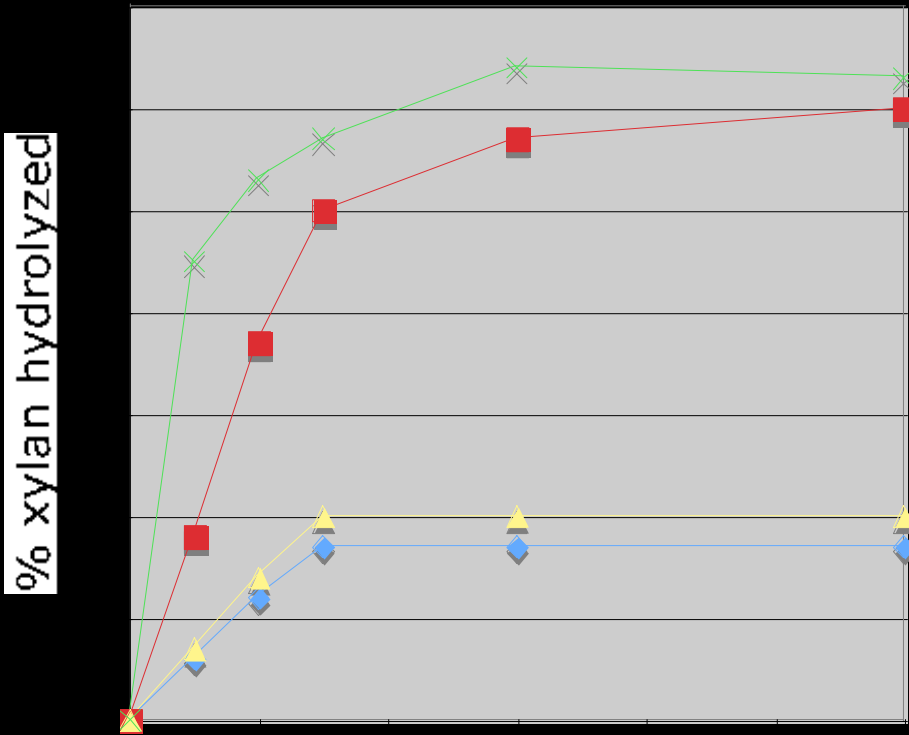
10%

Lignin S/G

2.1

6.5

Transgenic *Populus* wood with reduced lignin can be directly hydrolyzed by enzymes without chemical pretreatment



Theoretical ethanol yields from wildtype and transgenic *Populus* wood

Normal
wood

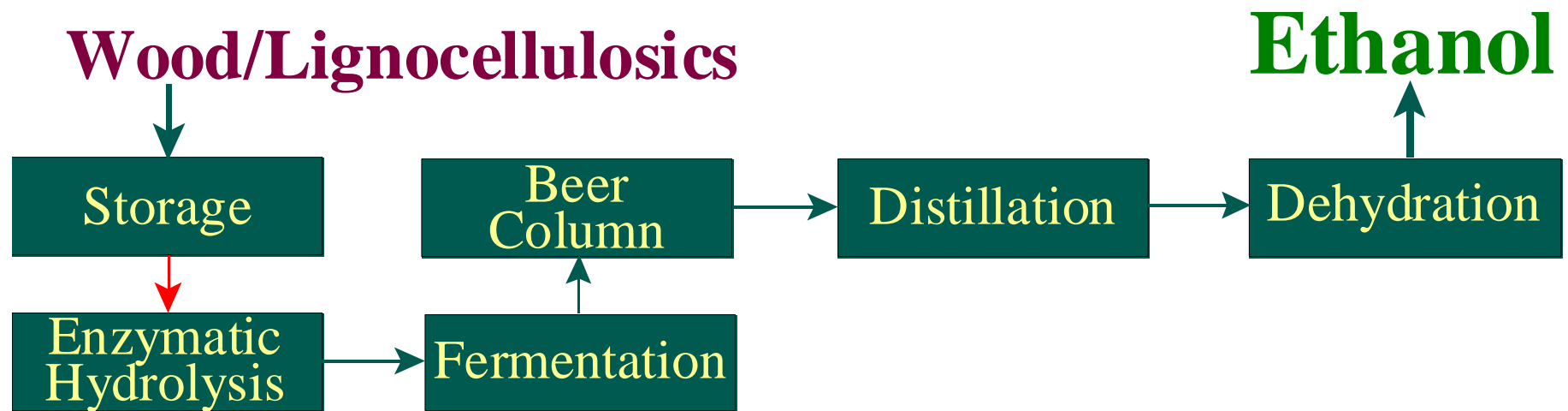
[13.6 gallon EtOH/ton wood]

Low lignin
wood

[99 gallon EtOH/ton wood]

Conversion of low lignin wood to ethanol (Direct enzymatic saccharification + fermentation)

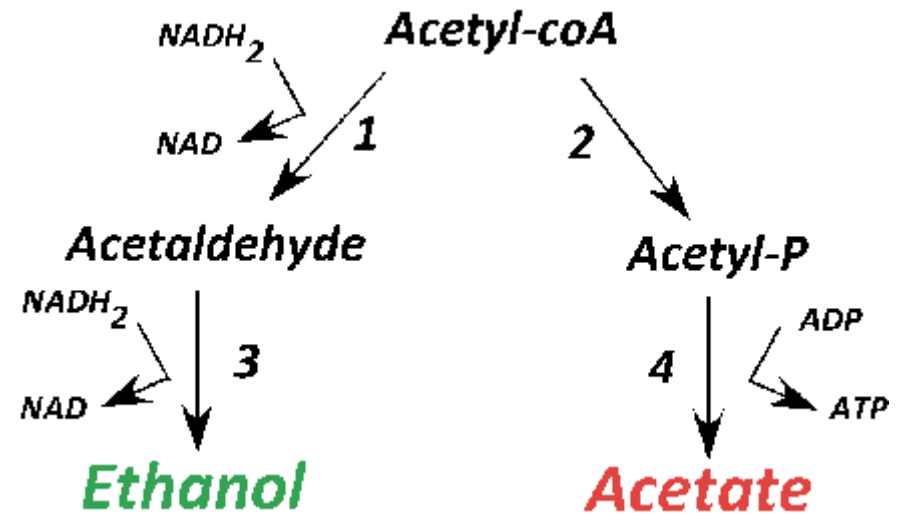
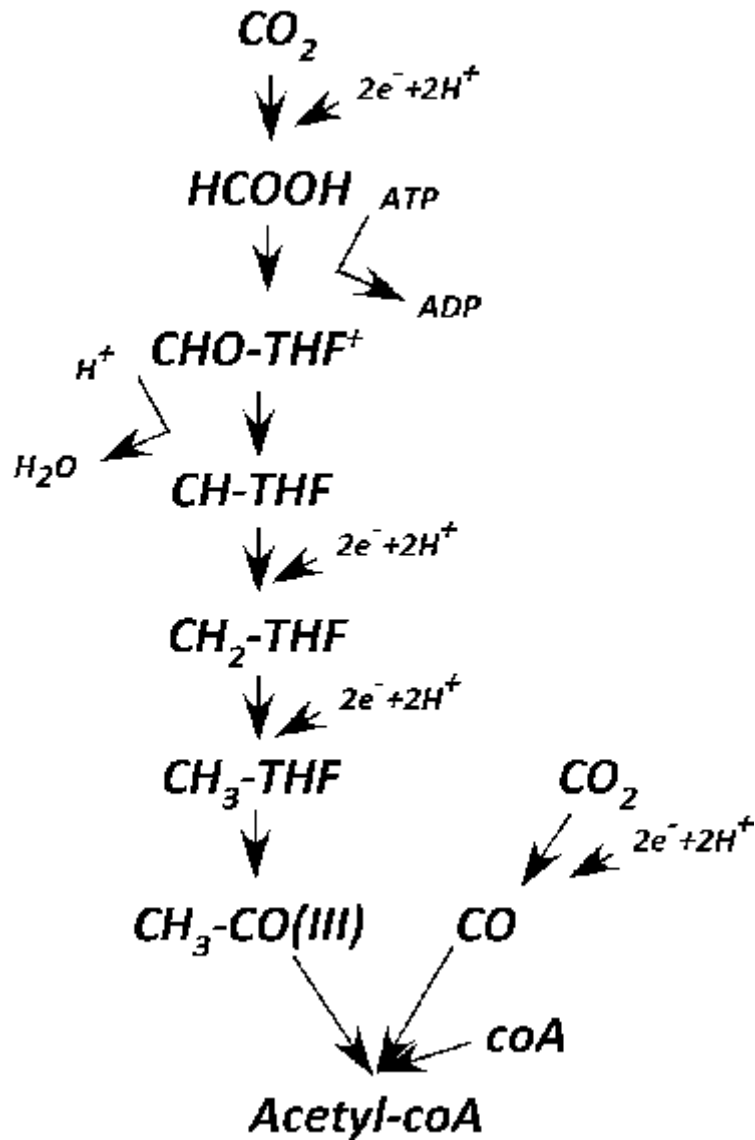
A process would be similar to current ethanol production from corn grain



Downstream processing: gas-phase CO_x adsorber capable of biofuel synthesis

- Advantages of microbial synthesis of ethanol from gas-phase CO_x (CO₂ or CO)
 - Recover gas-phase CO_x as useful fuel
 - Make C-C bonds from CO_x
 - CO_x can be from fermentation exhaust + H₂ or biomass gasification (syn-gas)
 - Less water use, better mass transfer than submerged syn-gas fermentation process
 - Higher total gas-phase carbon conversion efficiency to liquid fuel

Autotrophic acetogen/ethanologen (*Clostridia ljungdahlii*)

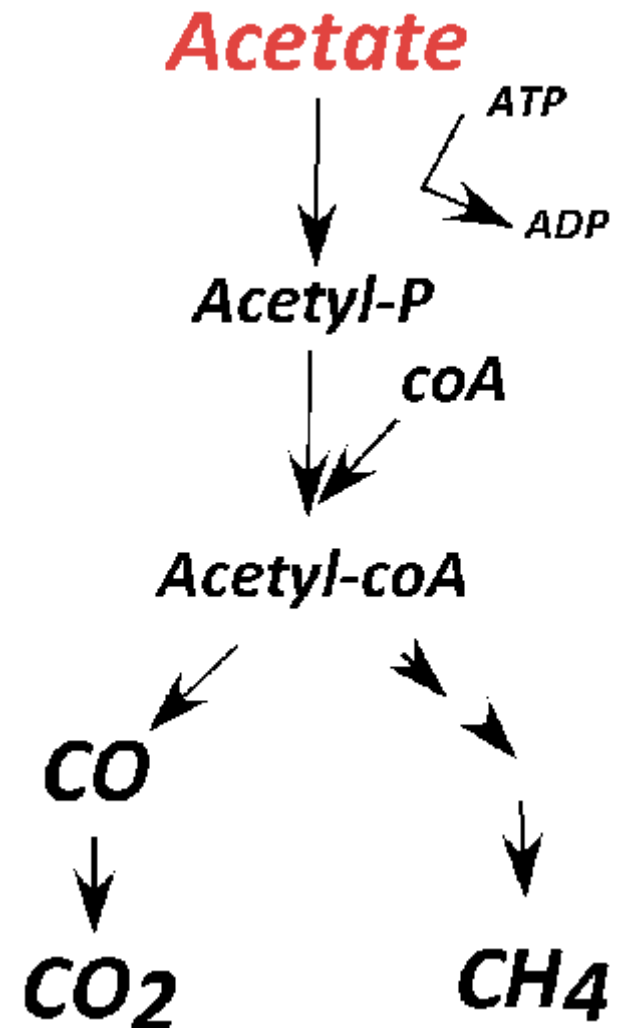


Anabolic pathway

1. Acetaldehyde dehydrogenase
2. Alcohol dehydrogenase
3. Phosphotransacetylase
4. Acetate kinase

Aceticlastic methanogen (Methanosaeta)

- Acetate is sole energy source
- Anaerobic
- Genome sequencing underway
- CO_2 and CO potential for recycle

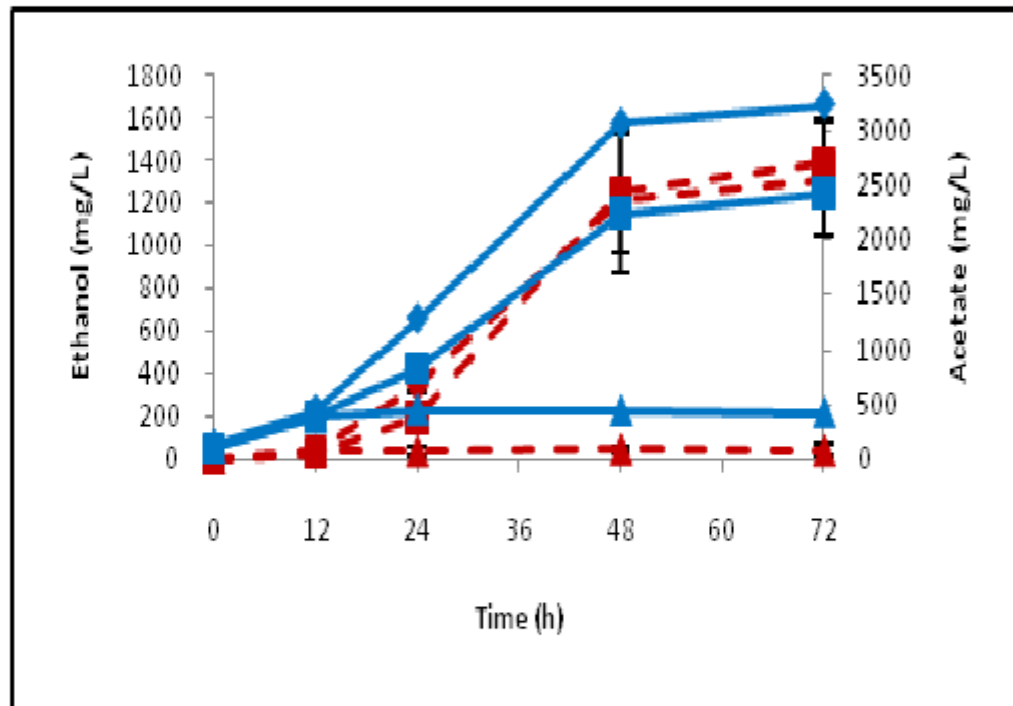


C. ljungdahlii –OTA1 vs. WT ethanol production on mRCMfs

- Reinforced Clostridial Medium with 5 g/L fructose in batch (50 ml media in 160 ml serum bottles) and reducing agents under 1 atm syngas (20 % CO₂, 20 % CO, 10 % H₂, 50 % N₂) (mRCMfs)
- Ethanol to acetate ratio

Time (h)	OTA1	WT
24	0.19	0.12
48	0.40	0.08
72	0.36	0.09

Results: *C. ljungdahlii*-OTA1 EtOH + Acetate Production in O₂ Exposed Cultures

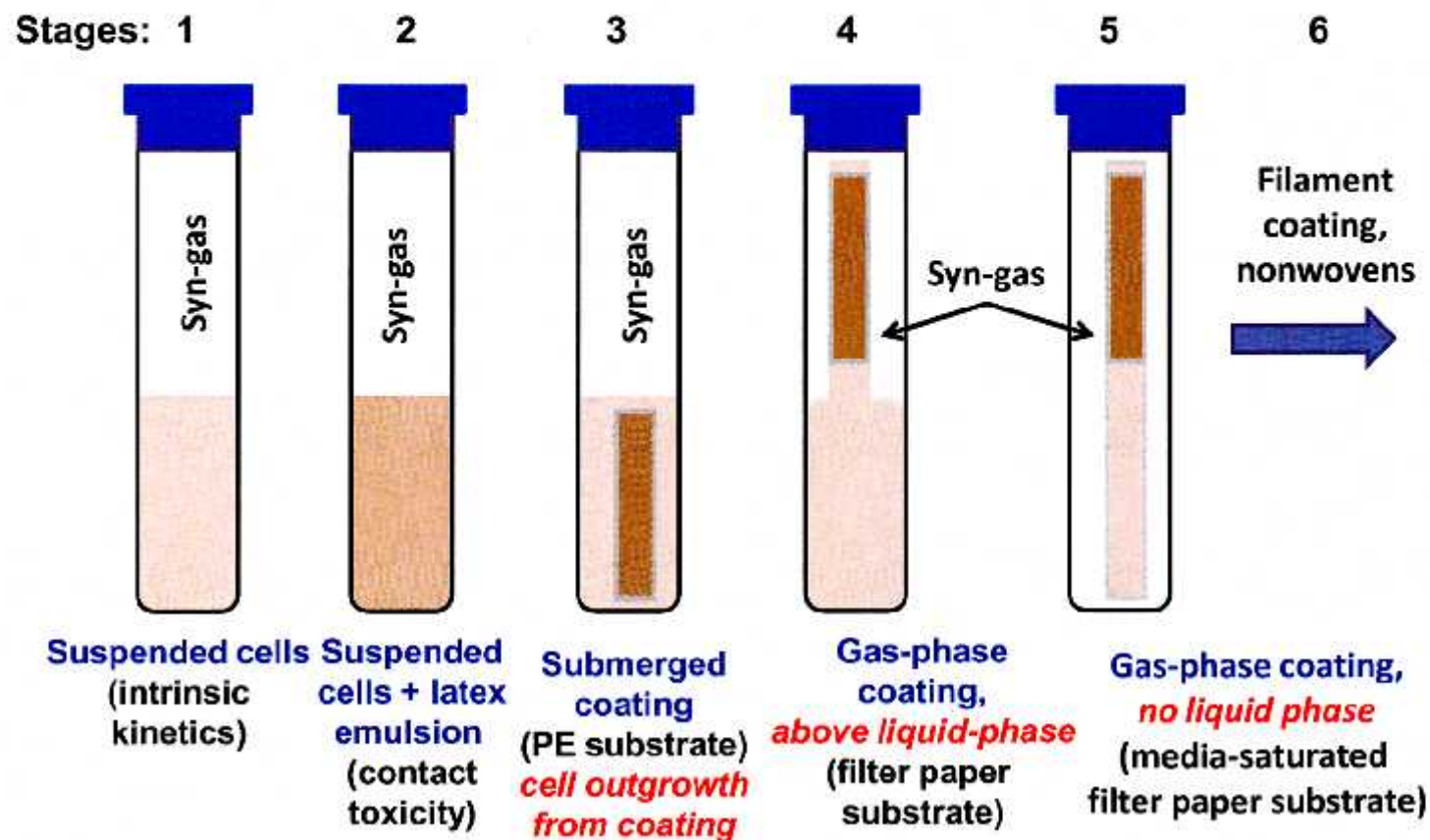


Ethanol to acetate ratios for *C. ljungdahlii*-OTA1 in control and oxygen exposed cells.

Time (h)	0 % O ₂	6 % O ₂	12 % O ₂
12	0.08	0.08	0.20
24	0.27	0.23	0.17
48	0.40	0.56	0.19
72	0.41	0.57	0.18

Dashed red lines, ethanol (diamond, 0 % O₂; square, 6 % O₂; triangle, 12 % O₂) Solid blue lines, acetate (diamond, 0 % O₂; square, 6 % O₂; triangle, 12 % O₂).

Stages in Development of *C. ljungdahlii* –OTA1 Latex Coatings for Gas-Phase Syn-Gas Conversion



Results: *C. ljungdahlii*-OTA1 Latex Coatings

- **Non-toxic latex coating emulsion, anaerobic coating methods developed**
 - Polyester coatings (non-porous substrate)
 - Media-saturated filter paper coatings
- **Media-submerged coatings consume syn-gas, produce EtOH, but demonstrate cell outgrowth** (sealant topcoat development needed)
- **Reproducible syn-gas consumption by coatings **above liquid-phase** and on saturated filter paper **without liquid-phase** demonstrated** (no outgrowth)
- **Gas-phase coating reactivity, EtOH + acetate yield** (experiments in progress)

Summary

- **Biochemical pathway manipulation**
 - **Has potential to improve ease of processing of material**
 - **Offers unique end products and product selectivity**
 - **Can reduce water utilization**
 - **Can improve biofuel yield**
 - **Is a productive tool in process engineering**